

Degradation of benzenesulfonate by heterogeneous photocatalysis combined with ozonation

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Abstract

The efficiency of the photocatalytic degradation of pollutants can be enhanced by combination with another advanced oxidation procedure such as ozonation. Application of these two methods for degradation of benzenesulfonate (BS) resulted in a synergic effect; the efficiency of the combined procedure significantly exceeded the sum of those of the individual techniques. Enhancement of the ozone dosage in this system accelerated the mineralization, i.e., the decrease of the total organic carbon content (TOC), more than the decay (transformation) of BS. The initial rates of both processes displayed a maximum at pH 5-6 in both the aerated and the ozonated systems. An increase of pH in the range of 2-7 promoted the mineralization in the ozonated system more than in the aerated one, while for the decay of BS a reversed relation was observed.

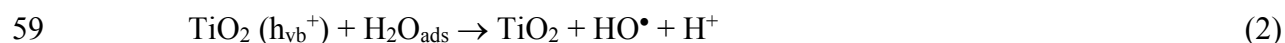
1. Introduction

The use of surface active compounds is widespread in several human activities. Among the anionic surfactants, alkanesulfonates, alkylsulfate, and alkylbenzenesulfonate are

35 commonly applied as cleaning agents, laundry detergents, cosmetics, and personal care
36 products [1]. The extensive use of these compounds leads also to their discharge into the
37 environment, mainly into the water compartment. Linear alkylbenzene sulfonates were
38 thoroughly investigated for their pollution effects and degradation possibilities, but less
39 studies dealt with benzene- and naphthalenesulfonates [2,3]. While the alkyl derivatives were
40 found to be readily biodegradable [4,5], other aromatic sulfonates without long side chains
41 proved to be biorecalcitrant [6]. Biodegradability of benzene- and naphthalenesulfonates with
42 sulfo, nitro and amino groups are especially low [7,8,9]. Due to their strong hydrophilic
43 character (low *n*-octanol–water partition coefficients [10]), low volatility and high mobility
44 within aquatic systems, polar aromatic sulfonates are easily transported from sewers to surface
45 waters. Hence they are potentially hazardous with respect to contamination of ground water
46 and drinking water supplies [11].

47 Various methods have been examined for the degradation of these contaminants in the
48 past two decades. Benzenesulfonates was mineralized by contact glow discharge electrolysis
49 [12, 13]. Ozonation was found to be efficient only in the presence of activated carbon, which
50 ensures high local concentration of the reactants through adsorption [14].

51 Photocatalytic procedures proved to be appropriate for purification of waters
52 contaminated with both inorganic and especially organic pollutants. In heterogeneous
53 photocatalytic methods applied for the degradation of various organic contaminants the most
54 widely used material is titanium dioxide, TiO₂ [3,15,16,17,18,19]. The determining oxidizing
55 species generated in TiO₂-mediated photocatalysis is hydroxyl radical, which is produced in
56 aqueous systems via oxidation of adsorbed water by the positively charged hole (h_{vb}⁺) formed
57 in the valence band of the semiconductor upon excitation (Eqs. 1, 2) [20].



60 In air-saturated systems, electrons (e_{cb}⁻) photogenerated in the conduction band can reduce
61 dissolved oxygen, leading to the formation of superoxide and peroxide ions (Eqs. 3, 4).



64 Procedures based on TiO₂-mediated photocatalysis were successfully applied for
65 degradation of various amino acids [21,22] and surfactants [3,19,23,24,25]. Efficient
66 photocatalytic mineralization of 1,5-naphthalenedisulfonate was also realized in titanium
67 dioxide suspension [26]. In this case, according to a detailed HPLC/MS analysis, the
68 degradation pathway leads to the formation and subsequent decay of benzenesulfonate.

69 Although the photocatalytic degradation of benzenesulfonate was studied in the past
70 [27,28], the possible degradation pathways in this system were just quite recently analyzed
71 [29].

72 Although TiO₂ based photocatalysis proved to be an efficient technique for degradation
73 of benzenesulfonate (abbreviated as BS) [29], its combination with another type of advanced
74 oxidation procedure can enhance the efficiency of its mineralization. In this study we
75 demonstrate that ozonation is an appropriate candidate for this purpose. Even if it was
76 successfully applied for degradation of BS only in the presence of activated carbon [14], its
77 combination with heterogeneous photocatalysis results in a synergistic effect in the increase of
78 the mineralization rate. Beside following the total organic carbon (TOC) content of the system
79 treated, monitoring of the concentration of both the starting material (BS) and its hydroxylated
80 derivatives was also carried out. The influence of the ozone dosage and the initial pH on the
81 degradation of BS has also been investigated in order to contribute to the elucidation of this
82 synergy. Beside their theoretical importance, the results of this work can be utilized in the
83 design of new catalytic procedures for wastewater treatment.

84

85 **2. Experimental Section**

86 **2.1. Materials**

87 In all experiments in this study, the titanium dioxide catalyst used was Degussa P25 (70%
88 anatase, 30% rutile; with a surface area of 50 m² g⁻¹). The concentration of TiO₂ was 1 g dm⁻³

89 in all cases. Reagent grade benzenesulfonic acid, 4-hydroxybenzenesulfonic acid, and 2,5-
90 dihydroxybenzenesulfonic acid (used as standards for the analyses) were purchased from
91 Merck. Compressed air was bubbled through the reaction mixtures from gas bottles both for
92 stirring and for serving (with its O₂ content) as electron acceptor. Beside dissolved oxygen
93 (O₂), in most of the experiments, O₃ (produced by a LAB2B ozone generator) was also
94 introduced in the same air stream. High purity water applied as solvent in this study was
95 double distilled and then purified with a Milli-Q system.

96

97 *2.2. Photochemical experiments*

98 Photochemical experiments were carried out in a laboratory-scale reactor with an
99 effective volume of 2.5 dm³. The heterogeneous reaction mixture (TiO₂ suspension) was
100 circulated by using a peristaltic pump through the reactor and the buffer vessel and by
101 continuously bubbling air with a flow rate of 40 dm³ h⁻¹ within the reactor. The photon flux of
102 the internal light source (40W, λ_{max} = 350 nm, i.e., UVA range) was measured by
103 tris(oxalato)ferrate(III) chemical actinometry [30,31] (I₀ = 4.3×10⁻⁶ mol photon dm⁻³ s⁻¹).

104

105 *2.3. Analytical procedures*

106 For analysis, 4 cm³ samples were taken from the reactors through a septum with a
107 syringe. When the solution part of the sample had to be analyzed, the solid phase was
108 removed by filtration using Millipore Millex-LCR PTFE 0.45 μm filters. The pH of the
109 aqueous phase of the reaction mixture was determined by a SEN Tix 41 electrode.

110 Mineralization was followed by measuring the total organic carbon (TOC) concentration,
111 utilizing a Thermo Electron Corporation TOC TN 1200 apparatus.

112 Benzenesulfonate and its hydroxylated intermediates were followed by HPLC-MS
113 measurements, the conditions of which were described earlier [29]. Sulfate anions were

114 analyzed by a Dionex DX300 ion chromatographic system (Dionex, Sunnyvale, CA, USA)
115 using suppressed conductivity detection. The injection volume was 50 μl . Separations were
116 carried out by a Dionex IonPac AS4A-SC (250 \times 4 mm) analytical column. The concentration,
117 pH and flow rate of the carbonate eluent were 3.5 mM, 10.2 and 1.2 ml min⁻¹.

118 The ozone concentration was determined by iodometry, using sodium iodide as reagent
119 and sodium thiosulfate for the titration of the iodine formed.

120

121 **3. Results and Discussion**

122 ***3.1. Mineralization of BS under various conditions***

123 In order to demonstrate the enhancement in the mineralization rate of BS by application
124 of the combined method (O₃/TiO₂/UV), the efficiencies of the simple individual methods
125 were also determined. Fig. 1 displays the change of TOC in systems containing BS of 10⁻³ M
126 initial concentration, during 300-min treatment by ozone alone, together with TiO₂ (in both
127 cases in the dark), as well as UV irradiated O₃, air/TiO₂, and O₃/TiO₂.

128 Insert Fig. 1 about here

129 As the corresponding plots indicate, that the mineralization efficiencies in systems O₃,
130 O₃/TiO₂, and O₃/UV are similar; TOC decreased about 31-32% during the 300-min irradiation
131 period. Apparently, neither TiO₂, nor UV-vis irradiation (here 320 – 420 nm) can significantly
132 affect the oxidation efficiency of ozone. The mineralization rate with irradiated TiO₂ in the
133 presence of dissolved oxygen (air/TiO₂/UV) was considerably higher than in the previous
134 cases, demonstrating the much more significant oxidation power of titanium dioxide based
135 photocatalysis. However, combination this method with ozonation (O₃/TiO₂/UV) increased
136 the mineralization efficiency much more than the simple addition of the efficiency of O₃ or
137 O₃/TiO₂ would result in. The initial mineralization rates summarized in Table 1 clearly

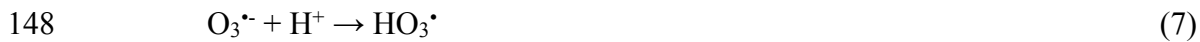
138 indicate this phenomenon: the initial rate with the combined method ($52.9 \times 10^{-2} \text{ mg dm}^{-3}$
139 min^{-1}) is about 1.6 times higher than the sum of the rates observed with the two individual
140 methods ($22.9 \times 10^{-2} + 9.8-11.2 \times 10^{-2} \text{ mg dm}^{-3} \text{ min}^{-1}$).

141 Insert Table 1 about here

142 Accordingly, in this case total mineralization was realized within 210-min irradiation.

143 A similar synergistic effect was observed by Li et al [32]. It can be interpreted by the
144 following reactions [33]:

145 - Direct electron transfer from TiO_2 to O_3 :



150 - Electron transfer between TiO_2 and O_2 molecule:



152 The electron scavenging by O_3 or O_2 decreases the possibility of the recombination of the
153 photogenerated electron-hole pair. Besides, formation of very oxidative radicals (e.g., in
154 reactions (6-8)) also enhances the degradation efficiency. Notably, UV irradiation of O_3 may
155 increase the amount of H_2O_2 and HO^{\bullet} species in the system.

156

157 ***3.2. Decay of BS and formation of sulfate under various conditions***

158 Beside the rate of the mineralization, other quantitative properties of the systems such
159 as the actual concentration of BS and sulfate ions were followed during the irradiations for
160 investigation if the manifestation of synergistic effect can be observed also in the change of
161 these species.

162 Insert Fig. 2 about here

163 A comparison of the initial decay rates of BS with those of the TOC regarding the whole
164 system clearly indicates that in the previous case the rate observed at the combined technique
165 ($O_3/TiO_2/UV$) does not exceed the sum of those of the individual methods (Figs. 1 and 2).

166 This result suggests that the synergistic effect originates from the efficient promotion of the
167 degradation of the intermediates formed during the decay of the starting material (BS).

168 However, as to the rate of the sulfate formation, the increasing effect of the ozonation is much
169 more pronounced, indicating that most of the sulfate ions in this system originated from the
170 intermediates, not from the starting material.

171

172 ***3.3. Formation and decay of intermediates in aerated and ozonated systems***

173 The actual concentrations of the starting material (BS) were directly determined from
174 HPLC-MS measurements. Thus, the TOC values corresponding to the unreacted
175 benzenesulfonate could also be calculated. Fig. 3A displays the TOC versus time plots
176 belonging to the overall system, the unreacted surfactant (BS), as well as the intermediates
177 formed during the photocatalytic degradation process in air-saturated system.

178 Insert Fig.3 about here

179 The latter curve is the difference of the previous two. The TOC values corresponding to the
180 intermediates show a maximum at 160-180 min where the concentration of the unreacted

181 benzenesulfonate is still considerable. At longer times (above 180 min) the TOC representing
182 the intermediates is diminishing because the rate of the mineralization of these species
183 exceeds that of their formation. In this period of irradiation, especially above 240 min, the
184 total TOC exclusively belongs to the intermediates because the whole amount of the starting
185 material (BS) has already been transformed. Hence, further decrease of TOC can be attributed
186 to the mineralization of the intermediates. In the presence of ozone (Fig. 3B) the decay of BS,
187 and, thus, the formation of the intermediates is much faster. Accordingly, the corresponding
188 plot shows the maximum TOC value belonging to the intermediates already at about 80 min,
189 and within 120 min all starting BS ions have been transformed. Also the total mineralization
190 took place within 210 min. Since the maximum values of TOC belonging to the intermediates
191 are about the same in both cases (air or ozone), the presence of O₃ accelerates both the
192 formation and the decay of these species.

193

194 ***3.4 The effects of ozone dosage***

195 The experiments with ozonated system, the results of which previously discussed were
196 carried out at constant O₃ dosage (0.12 mM min⁻¹), at less than half of the performance of the
197 ozone generator used. Thus, it was reasonable to investigate how the ozone dosage affects the
198 degradation of BS by using the combined procedure. Fig. 4 displays both the initial rate of the
199 BS decay ($V_0(\text{BS})$) and that of the mineralization, i.e., the TOC decrease ($V_0(\text{TOC})$), as
200 functions of the ozone dosage.

201 Insert Fig. 4 about here

202 It is clearly seen that the increase of $V_0(\text{TOC})$ is steeper than that of $V_0(\text{BS})$ at each value of
203 ozone dosage, and, what is more important, the ratio of these two rates gradually increases
204 upon increasing the O₃ dosage as shown by the data of Table 2.

205 Insert Table 2 about here

206 These data indicate that ozonation promotes the degradation of the intermediates stronger than
207 the transformation (hydroxylation) of the starting material does. A possible explanation of this
208 phenomenon may be that ozonation increases the steady-state concentration of superoxide in
209 this system more than that of the hydroxyl radicals because the latter species alone cannot open
210 the aromatic ring as it was proven in our previous work [29]. Ring-cleavage is an
211 indispensable step for the mineralization of BS .

212 All the three isomers of hydroxy-benzenesulfonate formed and decay during the degradation
213 of BS were followed by HPLC-MS measurements. In the absence of ozone the distribution of
214 the isomers at their maximum (total) concentration is the following: 16% *ortho*, 66 % *meta*,
215 and 18% *para*, in accordance with our earlier results (both theoretical [26] and analytical
216 [29]). Upon ozonation, the percentage of the *o*-hydroxy isomer did not significantly change
217 (14-17%), while that of the *meta* derivative decreased to 51%, with the increase of the *para*
218 species to 32-35 %). Interestingly, the change of the ozone dosage in the range of 0.011 – 0.35
219 mM min⁻¹ did not influence this distribution.

220

221 3.5. The effects of pH

222 The pH of this system determines the surface charge of the TiO₂ particles (pH_{Zpc} =
223 6.25 [34], and, thus, the adsorption efficiency of the benzenesulfonic acid, which is totally
224 dissociated (pK_{BS} = - 2.36 [14]) in the whole range of pH studied here. Besides, the
225 formations of the reactive oxidizing agents (e.g., HO•, O₂•-) as well as their reactions are also
226 affected by pH. Hence, V₀(BS) and V₀(TOC) were also measured as functions of the initial pH
227 (pH₀) in the range of 2.0 – 11.0, in both aerated and ozonated systems. According to our
228 results shown in Fig. 5, in aerated system the initial rate of both the BS decay and the
229 mineralization display maximum values at about pH 5-6.

230

Insert Fig. 5 about here

231 In the ozonated system the highest $V_0(\text{TOC})$ can be observed at the same pH as in the aerated
232 case, while the maximum of $V_0(\text{BS})$ is a bit lower pH value (ca. 4). These plots indicate that
233 not the adsorption of the determining factor affected by the pH in the range of 2-6, otherwise
234 the initial rate must increase upon acidification, due to the attraction between the positively
235 charged catalyst surface and the anionic benzenesulfonate and their derivatives. Thus, the
236 formation and reaction of the oxidizing agents are the key processes influenced by the pH in
237 these systems. In order to gain more information from these results, the ratios of the initial
238 rates (of both BS decay and TOC decrease) measured in ozonated and aerated photocatalytic
239 systems ($V_0(\text{O}_3)/V_0(\text{O}_2)$) were plotted as functions of pH_0 . As shown in Fig. 6, the
240 transformation of BS is less favored in the ozonated than in the aerated system upon
241 increasing pH values.

242 Insert Fig. 6 about here

243 This phenomenon can be partly attributed to the hindered formation of HO^\bullet radicals from
244 ozone because in these reactions ozonide ions are in protonated form (see reactions (5-8)).

245 On the contrary, for the ratio of the initial rates of mineralization, higher pH values (up
246 to about 7) are more favorable for the ozonated system, which may be explained by the
247 protonation of $\text{O}_2^{\bullet-}$, giving HO_2^\bullet being less efficient oxidizing agent than the superoxide
248 radical ($\text{pK}(\text{HO}_2^\bullet/\text{O}_2^{\bullet-}) = 4.8$ [35]). The latter species is the most probable reactant playing key
249 role in the ring-opening, which is indispensable for the mineralization of the aromatic
250 compounds.

251 .

252

253 **4. Conclusions**

254 In this study it has been demonstrated that the combination of titanium dioxide based
255 heterogeneous photocatalysis with ozonation for the oxidative degradation of

256 benzenesulfonate results in a synergistic effect, achieving a significantly higher mineralization
257 efficiency than the sum of those of the individual methods. Accordingly, this combination
258 offers an advantageous technique for purification of wastewaters. Since the optimum initial
259 pH for this joint procedure is just slightly acidic (i.e. close to neutral), this condition further
260 promotes the practical application of this combined method.

261

262 **Acknowledgments**

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266 2012-0071).

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270 **Figure captions**

271

272 **Fig. 1.** Change of total organic carbon (TOC) content as functions of time in the system
273 containing 1×10^{-3} M BS at $\text{pH}_0=3$ during the treatment by various oxidation methods: (\diamond) O_3 ,
274 (\blacklozenge) $\text{O}_3 + \text{TiO}_2$, (\blacktriangle) $\text{O}_3 + \text{UV}$, (\bullet) $\text{air} + \text{TiO}_2 + \text{UV}$, (\circ) $\text{O}_3 + \text{TiO}_2 + \text{UV}$. (TiO_2 content is 1 g dm^{-3}).

275 **Fig. 2.** Change of the concentration of the starting material (BS) (A) and SO_4^{2-} (B) as functions of
276 time in the system containing 1×10^{-3} M BS at $\text{pH}_0=3$ during the treatment by various oxidation
277 methods: (\blacktriangle) $\text{O}_3 + \text{UV}$, (\bullet) $\text{air} + \text{TiO}_2 + \text{UV}$, (\circ) $\text{O}_3 + \text{TiO}_2 + \text{UV}$. (TiO_2 content is 1 g dm^{-3}).

278 **Fig. 3.** Change of total organic carbon (TOC) content as functions of the irradiation time in the
279 system containing 1×10^{-3} M BS at $\text{pH}_0=3$ during the treatment by A) $\text{air} + \text{TiO}_2 + \text{UV}$ and B)
280 $\text{O}_3 + \text{TiO}_2 + \text{UV}$, indicating TOC belonging to the whole system (\bullet), the starting material (\circ), and
281 the intermediates formed (\blacktriangle). (TiO_2 content is 1 g dm^{-3}).

282 **Fig. 4.** The initial rate of BS decay (\bullet) and mineralization (\circ) as functions of ozone dosage in the
283 in the system containing 1×10^{-3} M BS at $\text{pH}_0=3$, treated by the combined procedure ($\text{O}_3 + \text{TiO}_2 +$
284 UV). (TiO_2 content is 1 g dm^{-3}).

285 **Fig. 5.** The initial rate of BS decay (A) and mineralization (B) as functions of pH_0 in the system
286 containing 1×10^{-3} M BS, treated by $\text{air} + \text{TiO}_2 + \text{UV}$ (\bullet) and $\text{O}_3 + \text{TiO}_2 + \text{UV}$ (\circ). (TiO_2 content is
287 1 g dm^{-3}).

288 **Fig. 6.** The ratio of the initial rates measured in ozonated and aerated system containing 1×10^{-3} M
289 BS as functions of pH_0 , regarding BS decay (\blacktriangle) and mineralization (\triangle). (TiO_2 content is 1 g
290 dm^{-3}).

291

292

293

294 **Table 1.** Initial rates of mineralization (i.e., the decrease of TOC) in the system containing 1×10^{-3}
295 M BS at $\text{pH}_0=3$ during the treatment by various oxidation methods.

Method	Initial rate / $\text{mg dm}^{-3} \text{ min}^{-1}$
O_3	10.0×10^{-2}
O_3/TiO_2	9.8×10^{-2}
O_3/UV	11.2×10^{-2}
Air/ TiO_2/UV	22.9×10^{-2}
$\text{O}_3/\text{TiO}_2/\text{UV}$	52.9×10^{-2}

296

297

298 **Table 2.** The ratios of the initial BS decay and mineralization rates at various ozone dosages in
299 the system containing 1×10^{-3} M BS at $\text{pH}_0=3$, treated by the combined method ($\text{O}_3/\text{TiO}_2/\text{UV}$).

Ozone dosage $V_0(\text{TOC})/V_0(\text{BS})$
(mM min^{-1})

0	29.8
0.011	30.7
0.016	35.3
0.12	37.5
0.35	44.3

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302 Fig. 1.

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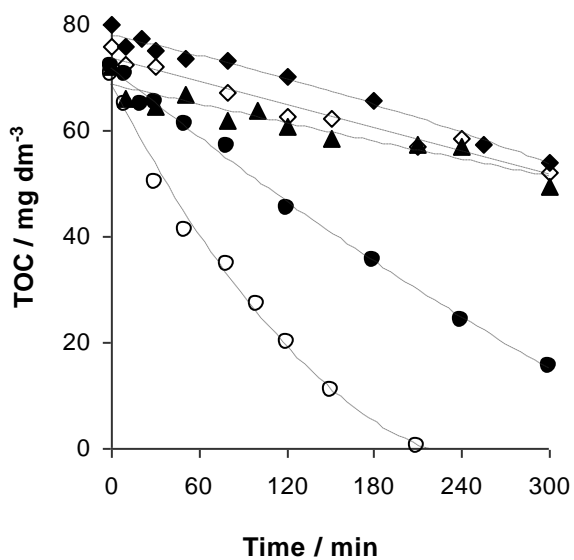
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316 Fig. 2.

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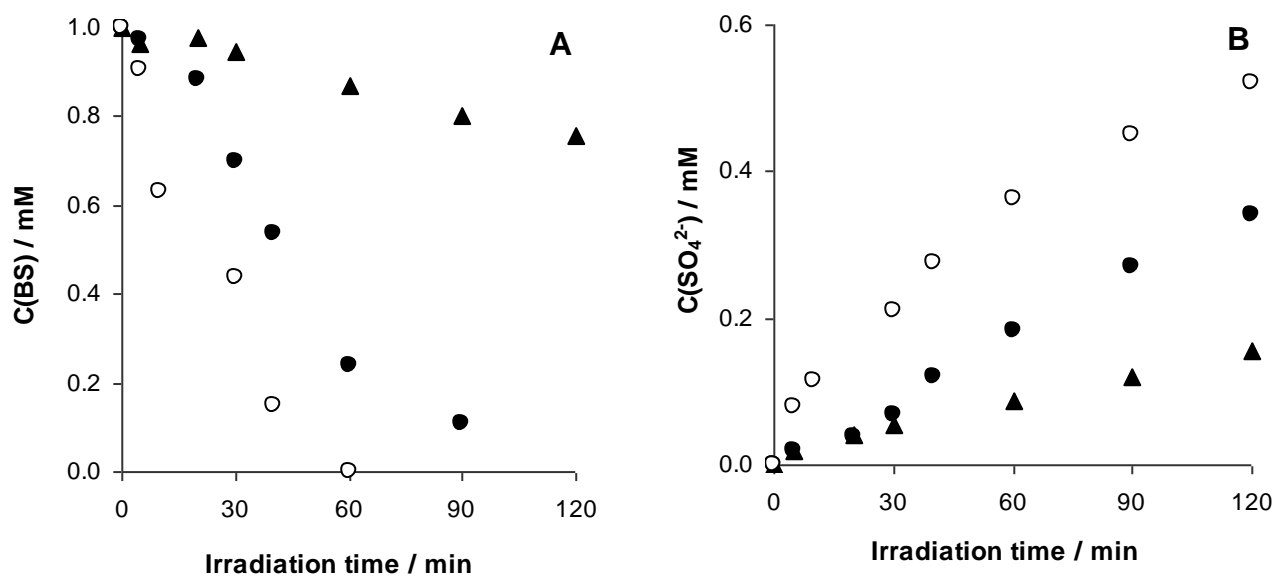
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328 Fig. 3.

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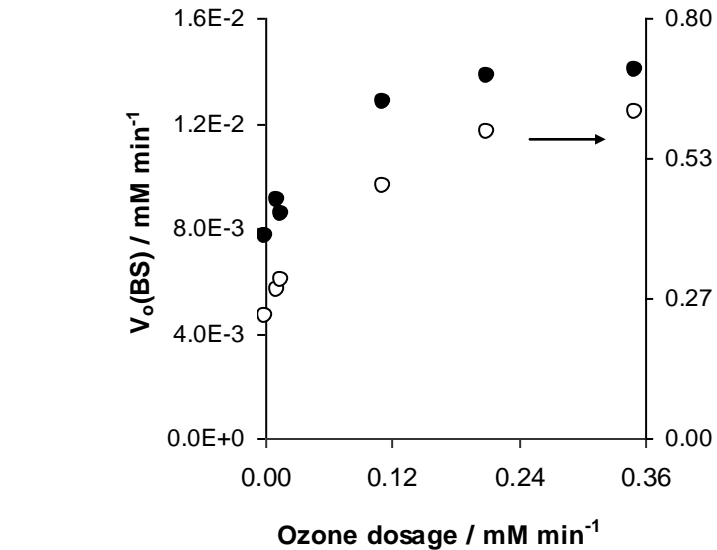
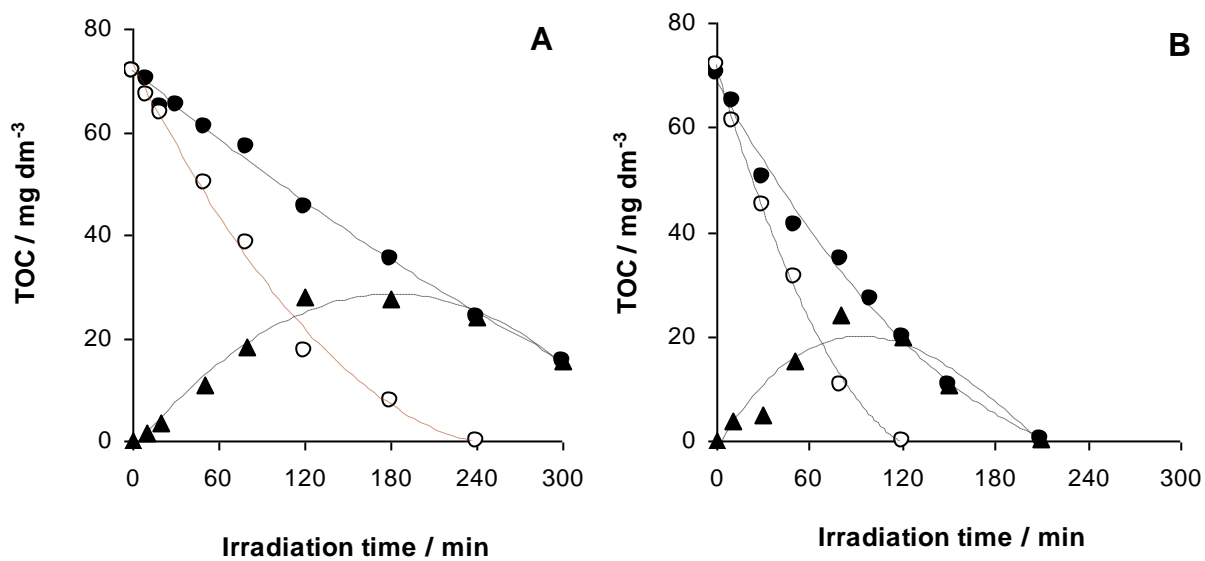
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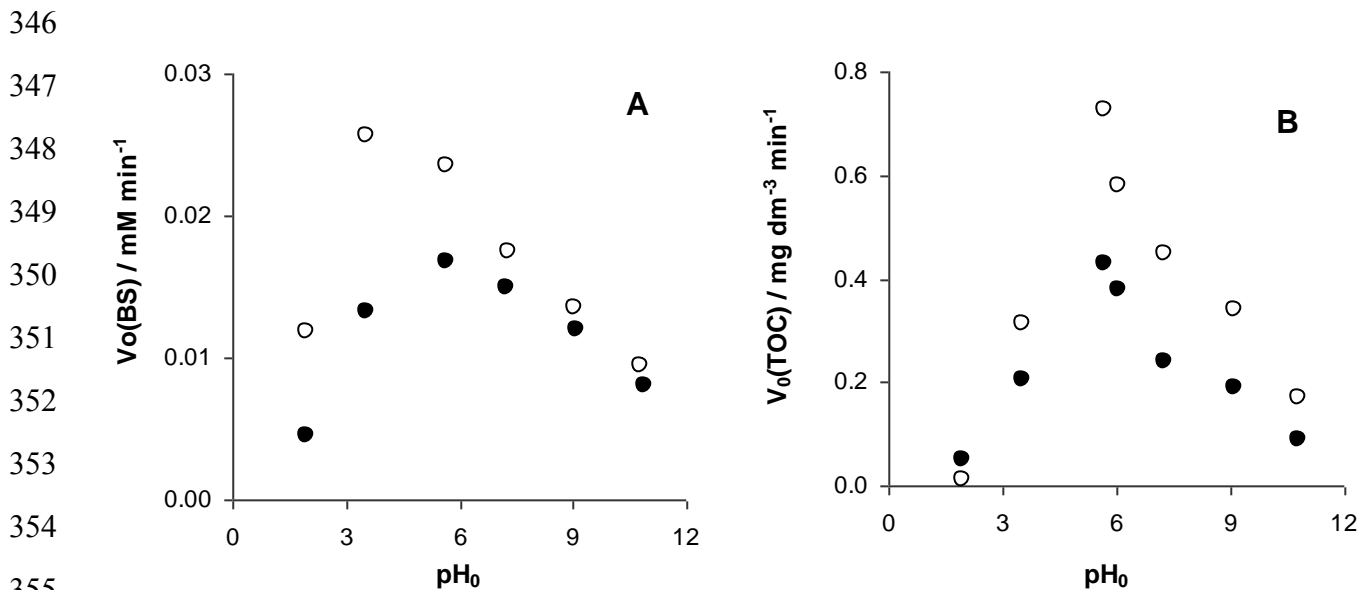
342 Fig. 4.



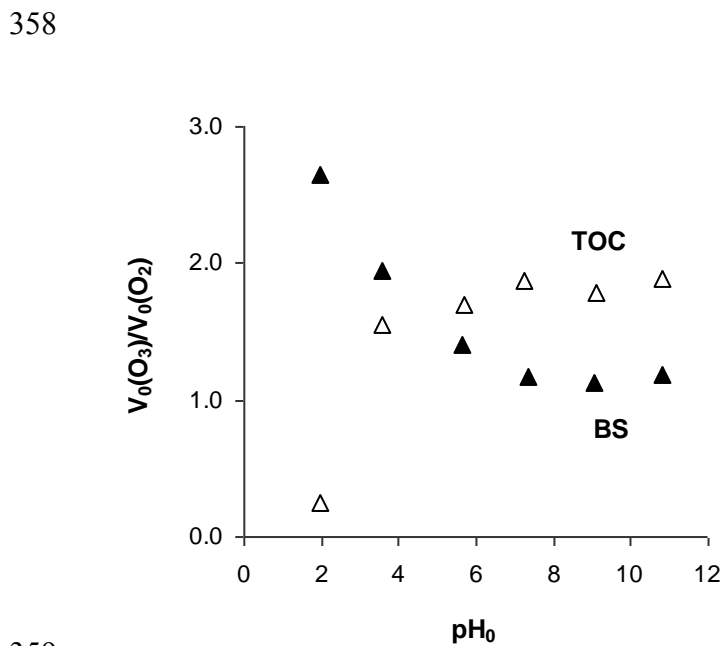
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345 Fig. 5.



357 Fig. 6.

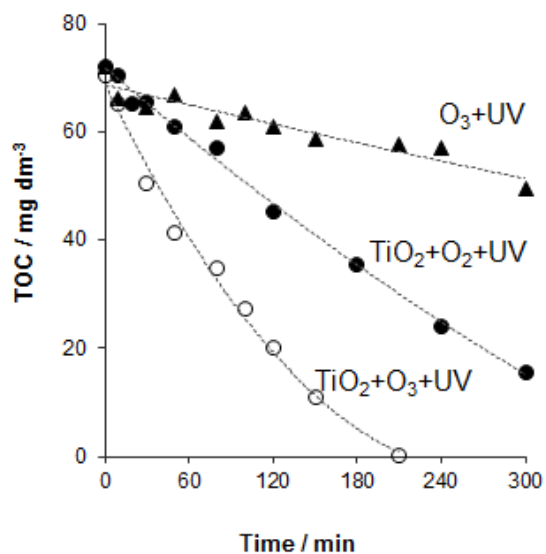


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361 Graphical abstract

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364 Application of TiO₂ based photocatalysis combined with ozonation for mineralization of
365 benzenesulfonate resulted in synergistic effect, achieving much higher efficiency than the sum of
366 those of the individual methods.

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