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9 **TiO₂ mediated photocatalytic mineralization of a non-ionic
10 detergent: comparison and combination with other advanced
11 oxidation procedures**

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22 **Abstract:** Triton X-100 is one of the most widely applied man-made non-ionic surfactants.
23 This detergent can hardly be degraded by biological treatment. Hence, a more efficient
24 degradation method is indispensable for the total mineralization of this pollutant. Application
25 of heterogeneous photocatalysis based on TiO₂ suspension is a possible solution. Its
26 efficiency may be improved by the addition of various reagents. We have thoroughly
27 examined the photocatalytic degradation of Triton X-100 under various circumstances. For
28 comparison, the efficiencies of ozonation and treatment with peroxydisulfate were also
29 determined under the same conditions. Besides, the combination of these advanced oxidation
30 procedures (AOPs) were also studied. The mineralization of this surfactant was monitored
31 by following the TOC and pH values, as well as the absorption and emission spectra of the
32 reaction mixture. An ultra-high-performance liquid chromatography (UHPLC) method was
33 developed and optimized for monitoring the degradation of Triton X-100. Intermediates
34 were also detected by GC-MS analysis and followed during the photocatalysis, contributing
35 to the elucidation of the degradation mechanism. This non-ionic surfactant could be
36 efficiently degraded by TiO₂-mediated heterogeneous photocatalysis. However,
surprisingly, its combination with the AOPs applied in this study did not enhance the rate of

37 the mineralization. Moreover, the presence of persulfate hindered the photocatalytic
38 degradation.

39 **Keywords:** nonionic surfactant; advanced oxidation process; titanium dioxide;
40 photocatalytic degradation; UHPLC; ozonation; persulfate

41

42 1. Introduction

43 In our natural waters, artificial detergents can threaten the self-cleaning processes such as
44 oxygen/carbon dioxide exchange and sedimentation of floating particles. As pollutants, through the
45 channel systems, they can get into our environment and may solubilize various water-insoluble
46 pesticides, polyaromatic hydrocarbons and other types of organic compounds [1-4]. These, along with
47 the surfactants themselves, may be toxic for microorganisms. A considerable part of synthetic detergents
48 is represented by non-ionic surfactants. They are more stable than ionic tensids, and not sensitive to the
49 pH and electrolytes of the aqueous systems in which they are involved. Currently, the non-ionic
50 surfactants of the alkylphenyl polyethoxylate type (Triton X-*n*) [5], where *n* can be within the range of
51 3-40, are the most widely used at the industrial scale. They are applied in household and industrial
52 cleaning agents, paints and coatings, as well as utilized in the dye and textile industries as detergents,
53 emulsifiers, wetting agents, solubilizers and dispersants [6-8]. Triton X-100 with an average *n* \approx 9.5 is
54 one of the most widespread man-made nonionic surfactants. Besides the hydrophilic polyethylene oxide
55 chain, it also contains a hydrophobic octylphenyl group.

56 In most large sewage farms, the degradation of organic pollutants takes place in biological systems
57 following physical preparation steps. However, Triton X-100 can hardly be degraded by biological
58 treatment under anaerobic conditions, and even in aerobic systems, it can be just partly mineralized in
59 this way [6-10]. Thus, as a consequence of the incomplete degradation, it can reach from the sewage
60 farms to natural waters, damaging the various living organisms there [11,12]. It may destroy the cell
61 membranes [13-15] and hinder the function of the peripheral nervous system [16]. Thus, they are
62 potentially hazardous with respect to the contamination of ground water and drinking water supplies
63 [17].

64 Hence, a more efficient degradation method is indispensable for the total mineralization of this
65 dangerous surfactant. Oxidation of the polyoxyethylene chain was carried out by using
66 $\text{Ag}^{\text{III}}(\text{H}_2\text{IO}_6)(\text{H}_2\text{O})_2$ (DPA) [18]. The primary products of this process were acetaldehyde and 4-(1,1,3,3-
67 tetramethylbutyl)phenol. Besides, various advanced oxidation processes (AOPs) were also applied for
68 the degradation of this detergent. Hydrated electron produced by pulse radiolysis, in the presence of *t*-
69 butanol, did not prove to be efficient enough [7,19]. Its reaction with various scavengers, such as O_2 and
70 N_2O , led to the formation of hydroxyl radicals, which oxidized the aromatic ring of the tenside via
71 hydrogen abstraction.

72 Heterogeneous photocatalysis based on titanium dioxide was also applied, but giving contradictory
73 results. At similar concentration of surfactant, the optimum catalyst concentrations found deviate by one
74 order of magnitude [20,21]. Modification of the photocatalyst with SiO_2 or Pt increased its activity by a
75 factor of two [22]. The addition of H_2O_2 or, especially, $\text{K}_2\text{S}_2\text{O}_8$ also increased the degradation efficiency

76 [21, 23] of the photocatalytic procedure. Different sources of UV light were used in these studies.
77 Besides, various 4-alkylphenols were also degraded by heterogeneous photocatalysis, but utilizing
78 visible light [24, 25]. The hydrophobic part of these complexes is very similar to that of the components
79 of Triton X-100. Intermediates were detected in these studies by LC-ESI-MS and GC-MS methods [23,
80 24], but the time dependence of their concentration was not followed.

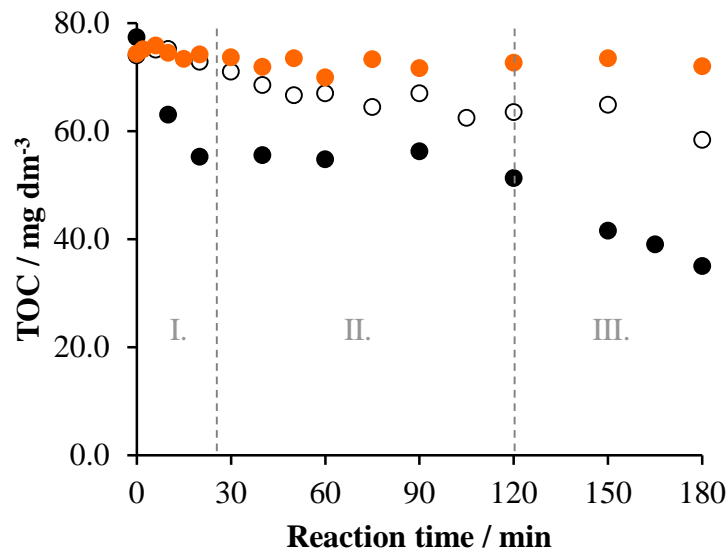
81 Our current investigations indicated TiO₂-mediated photocatalysis to be successfully applicable to
82 the mineralization of various ionic detergents [26-28] and amino acids [29]; besides, its combination
83 with ozonation resulted in a synergistic effect [30,31]. On the basis of the earlier, partly inconsistent
84 observations, our present paper deals with the oxidation and mineralization of Triton X-100 under
85 various circumstances, focusing on the heterogeneous photocatalysis, in order to get more insight into
86 the degradation mechanism. For comparison, the efficiencies of ozonation and treatment with
87 peroxydisulfate were also determined under the same conditions. Besides, the effects of the combination
88 of these advanced oxidation procedures (AOPs) were also investigated.

89 2. Results and Discussion

90 2.1. TiO₂/UV/air system

91 Before measuring the mineralization of Triton X-100 by heterogeneous photocatalysis, it was
92 investigated in the absence of the TiO₂ photocatalyst as well as without irradiation. As Figure 1 indicates,
93 no decrease of the TOC was observed during a 3-hour stirring with air-bubbling. Under the same
94 conditions, but irradiated at $\lambda_{ir} > 300$ nm, however, a moderate mineralization took place: 21%. The
95 initial rate of the TOC decrease was $0.26 \text{ mg dm}^{-3} \text{ min}^{-1}$. This result indicates that also a direct photolysis
96 of the surfactant can happen in the aerated system, which may be attributed to the excitation of the
97 tenside due to the slight overlap of its absorption spectrum and the emission spectrum of the UV light
98 source applied. In the presence of 1 g dm^{-3} TiO₂ photocatalyst, the initial rate and the extent of
99 mineralization significantly increased (to $1.75 \text{ mg dm}^{-3} \text{ min}^{-1}$ and 55%, respectively). Besides, the TOC
100 *versus* reaction time function can be divided into three unambiguously distinguishable sections (Figure
101 1).

102 **Figure 1.** The change of the TOC as a functions time under various conditions in the system
103 containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and 1 g dm^{-3} TiO₂: air (●), air/UV (○), air/UV/TiO₂ (●).



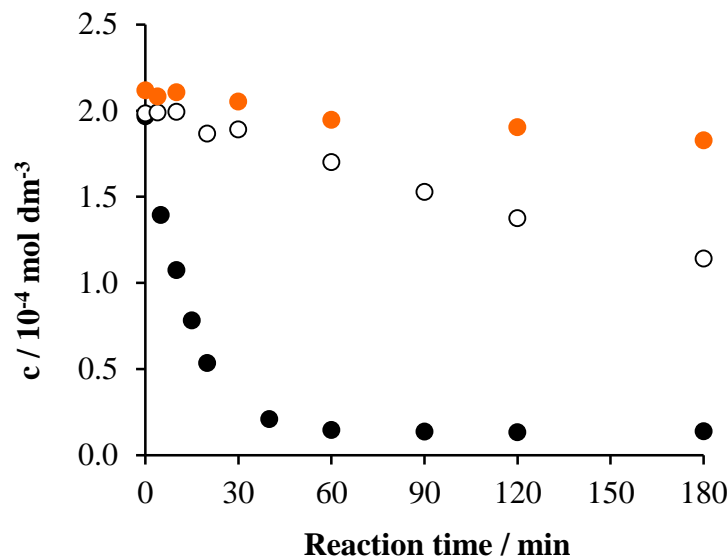
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105

106 In the first 20 min, the TOC decreased quickly, from 74 mg dm⁻³ to 58.4 mg dm⁻³. However, in the
 107 subsequent 100-min period, practically no change of the TOC took place. This result suggests that only
 108 intermediates (oxidized derivatives) were formed during this period, without any mineralization. In the
 109 last 60 min, the TOC decreased again, although at a lower rate (0.67 mg dm⁻³ min⁻¹) than initially. In
 110 this period, mineralization of the intermediates formed in the initial stage took place. The pH of the
 111 reaction mixture changed from 5.9 to 3.2 during the 3-h irradiation.

112 The actual concentration of the surfactant was followed by UHPLC during the reaction time. The
 113 results are shown in Figure 2.

114 **Figure 2.** The change of the Triton X-100 concentration as a function of the reaction time
 115 under various conditions in the system containing 2×10⁻⁴ mol dm⁻³ Triton X-100 and 1 g dm⁻³
 116 ³TiO₂: air (●), air/UV (○), air/UV/TiO₂ (●).

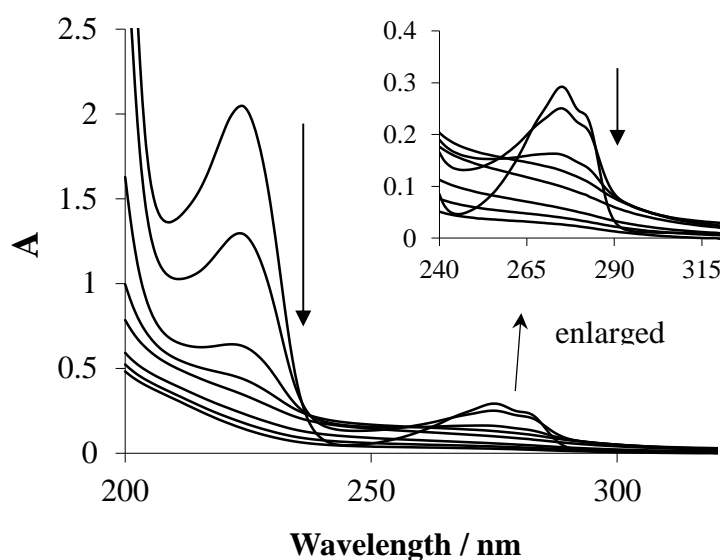


117

118 In accordance with the TOC *versus* time plots (Figure 1), no appreciable change was observed without
119 irradiation, while in the irradiated system (in the absence of the catalyst) a 42.5% decrease took place at
120 an initial rate of $6 \times 10^{-7} \text{ mol dm}^{-3} \text{ min}^{-1}$. This result indicates that this surfactant, even if to a moderate
121 extent, can be transformed under natural conditions, upon solar irradiation. In the presence of TiO_2
122 photocatalyst, the concentration of the starting tenside diminished below the detection limit within the
123 first hour of irradiation (Figure 2). The initial rate of its disappearance was $10^{-5} \text{ mol dm}^{-3} \text{ min}^{-1}$,
124 unambiguously demonstrating an efficient transformation of this pollutant. The decrease of the detergent
125 concentration in the photocatalytic degradation obeyed first-order kinetics (Figure S1), in accordance
126 with earlier observations [20, 21, 23]. However, instead of the apparent rate constants, the initial rates
127 were used for comparison, because the kinetics of the decay was not unambiguously first order in the
128 case of the thermal reactions.

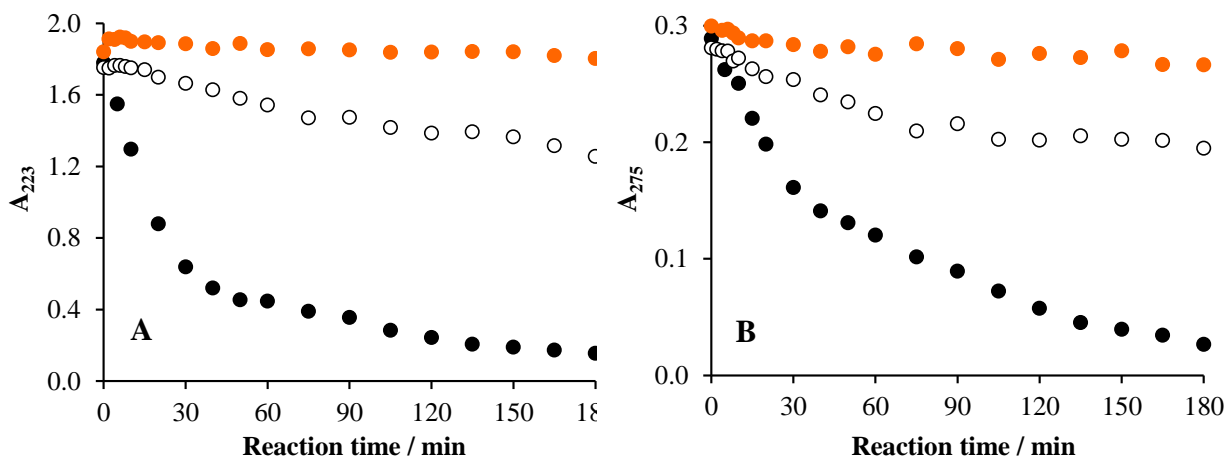
129 Furthermore, also the change of the absorption spectrum displayed the degradation of Triton X-100
130 in the latter system (containing TiO_2). As Figure 3 shows, the model compound displays two intense
131 bands in the 200–350-nm range; one at 210–240 nm and another one at 250–290 nm. The latter band
132 can be assigned to the $\pi \rightarrow \pi^*$ transition characteristic of the aromatic system. During the degradation
133 process, the absorbances of both bands gradually decreased.
134

135 **Figure 3.** The change of the absorption spectrum (after removal of the suspended TiO_2)
136 during the photocatalysis in the aerated system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and
137 1 g dm^{-3} catalyst ($\ell = 1 \text{ cm}$).
138



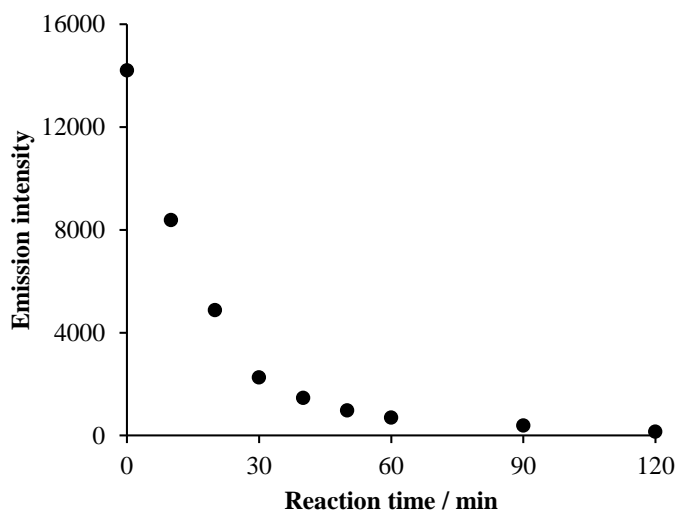
139 Surprisingly, no shift of the absorption bands was observed, which suggests that no hydroxylation
140 precedes the ring opening. Figure 4 displays the absorbance *versus* reaction time plots under various
141 conditions at the characteristic wavelengths (223 and 275 nm).
142
143

144 **Figure 4.** The change of the absorbance at 223 nm (A) and 275 nm (B) as a function of the
145 reaction time under various conditions in the system containing 2×10^{-4} mol dm⁻³ Triton X-
146 100 and 1 g dm⁻³ TiO₂ ($\ell = 1$ cm): air (●), air/UV (○), air/UV/TiO₂ (●).
147



148 In accordance with the concentration *versus* time plots, negligible change was observed without
149 irradiation, while direct photolysis caused a moderate, but continuous, decrease of the absorbance at 223
150 nm. However, at 275 nm in the 90–120-min range, no significant change can be observed, indicating
151 that at this wavelength, relatively stable intermediates formed display absorption. In the case of the
152 photocatalytic degradation, much faster and continuous decreases of absorbance are shown, but at 223
153 nm, the rate of the absorption change is significantly higher than at 275 nm. This phenomenon, in
154 accordance with the conclusion regarding the direct photolysis, suggests that the absorption at the latter
155 (longer) wavelength can be attributed to more stable intermediates than those absorbing at 223 nm.
156 Besides, the change of the intensity of emission originating from the aromatic moiety of the molecules
157 indicates that, already in the early stage of the photocatalytic degradation, a significant part of the
158 benzene rings was destroyed (Figure 5), in accordance with the observations regarding alkylphenols in
159 very similar systems [24]. The decay of this emission proved also to be of first-order kinetics (Figure
160 S2). Similarly to the absorption spectra, no band-shift was observed during the irradiation, indicating
161 that no significant hydroxylation of the aromatic ring occurred. Notably, in argon-saturated reaction
162 mixture, TiO₂-based photocatalysis cannot lead to the cleavage of the aromatic ring, and only emissive
163 hydroxylated derivatives are formed [26, 28].
164

165 **Figure 5.** The change of the emission intensity (after removal of the suspended TiO_2) during
166 the photocatalysis in the aerated system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and 1 g
167 dm^{-3} catalyst ($\ell = 1 \text{ cm}$, $\lambda_{\text{ex}} = 277 \text{ nm}$, $\lambda_{\text{em}} = 302 \text{ nm}$).



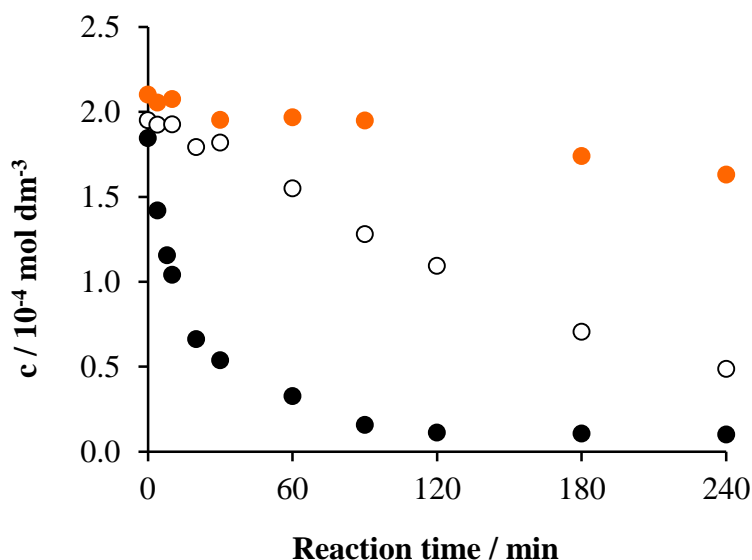
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169 2.2. Effects of $\text{Na}_2\text{S}_2\text{O}_8$

170 Regarding the effects of oxidative additives, firstly application of peroxydisulfate (or persulfate) was
171 investigated: in the dark ($\text{Na}_2\text{S}_2\text{O}_8/\text{air}$), irradiated ($\text{Na}_2\text{S}_2\text{O}_8/\text{air}/\text{UV}$), and combined with heterogeneous
172 photocatalysis ($\text{Na}_2\text{S}_2\text{O}_8/\text{air}/\text{UV}/\text{TiO}_2$). Since persulfate is an efficient oxidizing agent in thermal
173 processes, 22% decrease of the surfactant concentration was observed after a 4-hour reaction time, with
174 $2 \times 10^{-7} \text{ mol dm}^{-3} \text{ min}^{-1}$ initial rate (Figure 6). No change of the pH accompanied this process.

175

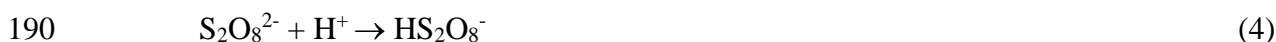
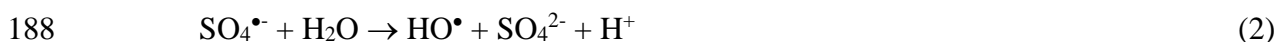
176 **Figure 6.** The change of the Triton X-100 concentration as functions of the reaction time
177 under various conditions in the system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and
178 $10^{-3} \text{ mol dm}^{-3} \text{ Na}_2\text{S}_2\text{O}_8$: air (●), air/UV (○), air/UV/ TiO_2 (1 g dm^{-3}) (●).



179

180 Upon irradiation of this system, under the same conditions as in the dark, considerably higher
 181 concentration decrease (76%) was observed, and, accordingly, 4 times higher initial rate (8×10^{-7} mol
 182 $\text{dm}^{-3} \text{min}^{-1}$). Notably, this concentration decrease is about the sum of those observed for the air/UV and
 183 $\text{Na}_2\text{S}_2\text{O}_8/\text{air}$ systems after 4 hours (54%+22%). The pH significantly changed (from 5.4 to 3), which
 184 may be the consequence of H^+ formation in the reactions of sulfate radical-anion ($\text{SO}_4^{\bullet-}$) generated (Eqs.
 185 1-5) [32].

186

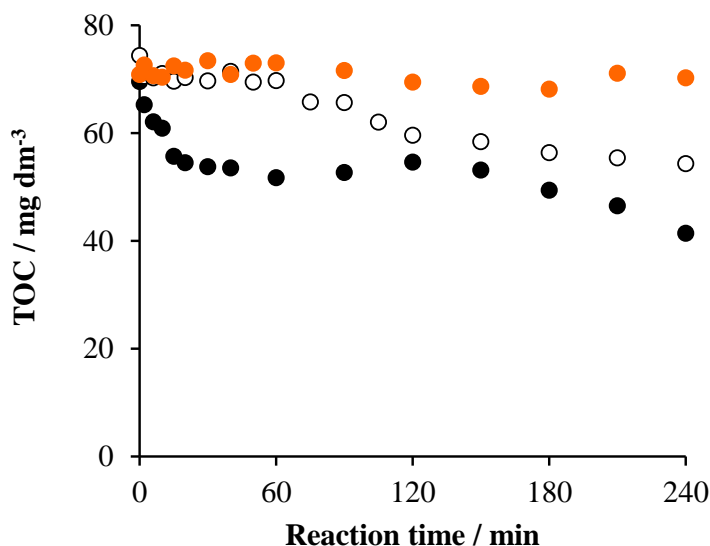


192 Since the photoinduced dissociation of persulfate (Eq. 1), however, needs excitation at wavelengths
 193 shorter than 310 nm, our light source hardly promote this reaction. The thermal reactions between
 194 persulfate and the excited surfactant, the formation of which is indicated by the results of the direct
 195 photolysis (see in Section 2.1.), can give a more significant contribution to the acidification. In the
 196 system containing photocatalyst too, the concentration of Triton X-100 decreased below the detection
 197 limit within about 90 min (Figure 6). The initial rate was $10^{-5} \text{ mol dm}^{-3} \text{ min}^{-1}$, which agrees with that
 198 observed for the photocatalytic degradation in the absence of persulfate. This result indicates that,
 199 deviating from earlier observations [21, 23], addition of persulfate did not increase the efficiency of the
 200 degradation of Triton X-100. The different light sources used are the main reason for this deviation.
 201 While in this study the light tube emitted at 350 nm, in the previous works irradiations at much shorter
 202 wavelengths were applied, e.g., 254 nm in ref. 23. Thus, reaction (1) efficiently took place in those
 203 experiments, while the energy of our light source was not enough for that process. Moreover, in our case,
 204 addition of persulfate apparently hindered the photocatalytic process as the corresponding plots in
 205 Figures 2 and 6 demonstrate. This phenomenon may be attributed to the occupation of the active sites

on the surface of the catalyst by the persulfate ions or sulfate ions formed from the previous ones. Due to the more effective oxidative degradation in the presence of TiO_2 , the acidification is one order of magnitude higher than in the system without photocatalyst; the pH changed from 5.4 to 2.

Comparing the mineralization efficiencies (i.e., the TOC vs. time plots), the tendencies are similar to those observed for the decrease of the surfactant concentration. As Figure 7 displays, no change of the TOC happened in the dark, while a moderate but continuous decrease took place in the irradiated system without catalyst, with $0.01 \text{ mol dm}^{-3} \text{ min}^{-1}$ initial rate and 27% mineralization (within 4 hours). The presence of the photocatalyst increased the initial rate by two orders of magnitude ($1.07 \text{ mol dm}^{-3} \text{ min}^{-1}$) and the mineralization to 40%. However, these values are considerably lower than the corresponding ones observed for the heterogeneous photocatalysis in the absence of persulfate (55% and $1.75 \text{ mol dm}^{-3} \text{ min}^{-1}$), confirming the hindering effect also observed for the decrease of the surfactant concentration. This contrast with the earlier observations [21, 23] may be attributed to the different conditions; e.g., two orders of magnitude lower concentration of TiO_2 was applied in those experiments [21] than in the present work, also the intensities and the emission spectra of the light sources were considerably different as indicated above. Besides, in our study, the concentration of the detergent was about one order of magnitude higher than those in the previous works.

Figure 7. The change of TOC as functions of the reaction time under various conditions in the system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and $10^{-3} \text{ mol dm}^{-3}$ $\text{Na}_2\text{S}_2\text{O}_8$: air (●), air/UV (○), air/UV/ TiO_2 (1 g dm^{-3}) (●).

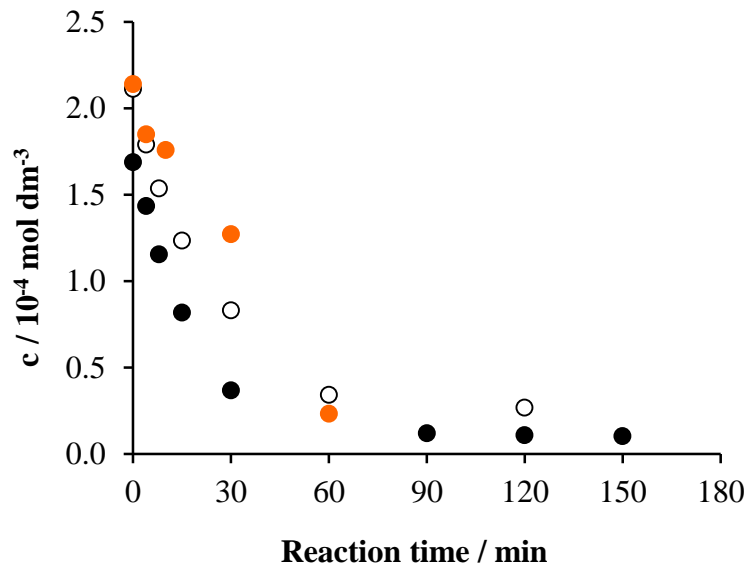


2.3. Effects of ozonation

Ozone was generated in the air stream bubbled through the reaction mixture at $40 \text{ dm}^3 \text{ h}^{-1}$ rate. The input ozone current was $3.5 \times 10^{-4} \text{ mol dm}^{-3} \text{ min}^{-1}$. Also in this case, experiments under three different conditions were carried out: in the dark (O_3/air), irradiated ($\text{O}_3/\text{air}/\text{UV}$), and combined with heterogeneous photocatalysis ($\text{O}_3/\text{air}/\text{UV}/\text{TiO}_2$). Like persulfate, ozone is also an efficient oxidizing agent in thermal processes. Accordingly, the concentration of the surfactant decreased below the detection limit within an hour, with an initial rate of $2 \times 10^{-6} \text{ mol dm}^{-3} \text{ min}^{-1}$ (Figure 8). Irradiation and

234 photocatalysis accelerated transformation of Triton X-100; the initial rate became tripled in in these
 235 cases ($6 \times 10^{-6} \text{ mol dm}^{-3} \text{ min}^{-1}$).

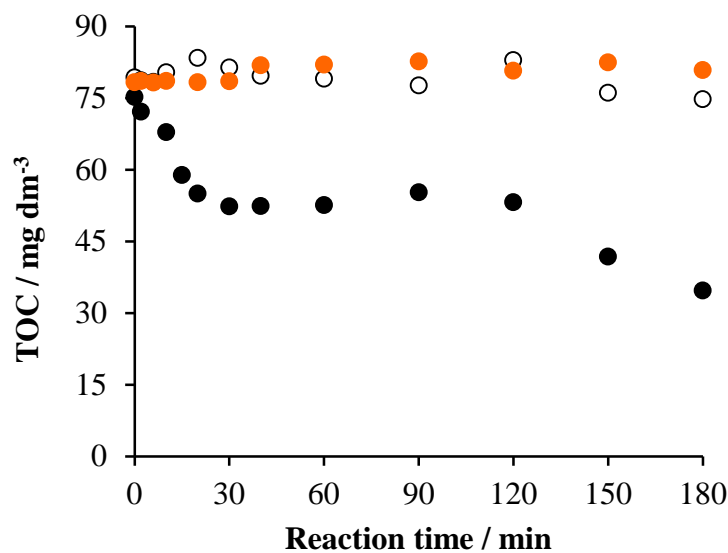
236 **Figure 8.** The change of the Triton X-100 concentration as functions of the reaction time
 237 under various conditions in the system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and
 238 ozonated at $3.5 \times 10^{-4} \text{ mol dm}^{-3} \text{ min}^{-1}$ rate: air (●), air/UV (○), air/UV/TiO₂ (1 g dm⁻³) (●).



239

240 Regarding the mineralization of Triton X-100 by ozonation, no change of the TOC was observed
 241 without irradiation and, deviating from the case of persulfate, the concentration of the total organic
 242 carbon did not appreciably decrease even in the irradiated system (O₃/air/UV) as shown in Figure 9.

243 **Figure 9.** The change of the TOC as functions of the reaction time under various conditions
 244 in the system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and ozonated at $3.5 \times 10^{-4} \text{ mol dm}^{-3}$
 245 min⁻¹ rate: air (●), air/UV (○), air/UV/TiO₂ (1 g dm⁻³) (●).



246

247 These data, compared to those in Figure 8, indicate that the considerable transformation (oxidation) of
 248 the surfactant in the O₃/air and O₃/air/UV systems resulted in the formation of intermediates, which did
 249 not mineralize at all during the 3-hour reaction time. Combination with photocatalysis led to the same

250 mineralization efficiency (54%) as in the case of the air/UV/TiO₂ system, and to an initial rate (1.44 mg
 251 dm⁻³ min⁻¹), which is just slightly lower than the corresponding value measured without ozonation. These
 252 data suggest that ozonation, deviating from our observations regarding ionic surfactants [30,31], does
 253 not increase the efficiency of the photocatalytic mineralization of Triton X-100. However, contrary to
 254 persulfate, O₃ does not show any significant hindering effect either, probably because it cannot occupy
 255 the active sites on the surface of the catalyst.

256

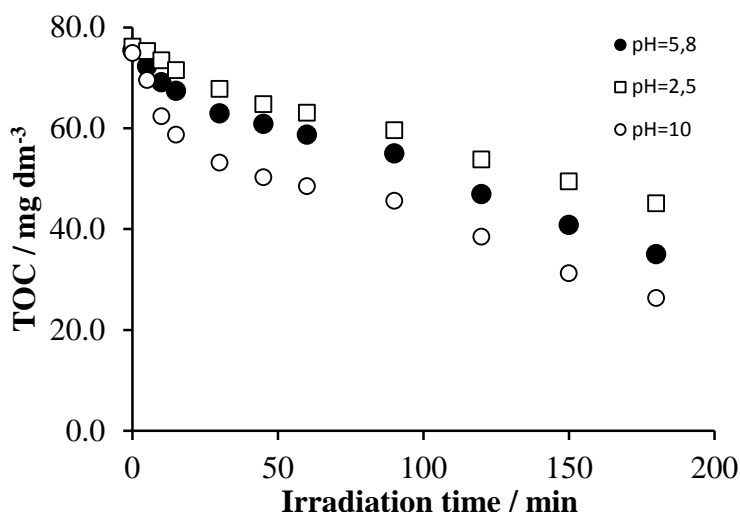
257 2.4. Effects of the initial pH

258 According to recent observations, pH considerably affects the rate of the primary oxidation of Triton
 259 X-100 in the TiO₂-based photocatalytic degradation [23]. Those results indicated that the pH values
 260 where the catalyst surface is close to neutral are favorable for the reaction, promoting the adsorption of
 261 the non-ionic surfactant. Thus, pH values near to that of the isoelectric point (IEP) of titania (6.8 [33])
 262 are most suitable in this respect. This conception is in accordance with the Langmuir-Hinshelwood
 263 model, the primary oxidation reaction of Triton X-100 was found to obey [23]. However, the
 264 mineralization of this detergent, i.e., the decrease of the TOC of its solution, does not necessarily follow
 265 this tendency. As Figure 10 displays, the pH effect on the mineralization rate of Triton X-100 is different
 266 from that regarding its primary oxidation step.

267

268 **Figure 10.** The change of the TOC as functions of the irradiation time at various pH values
 269 in the aerated system containing 2×10^{-4} mol dm⁻³ Triton X-100 and 1 g dm⁻³ TiO₂.

270



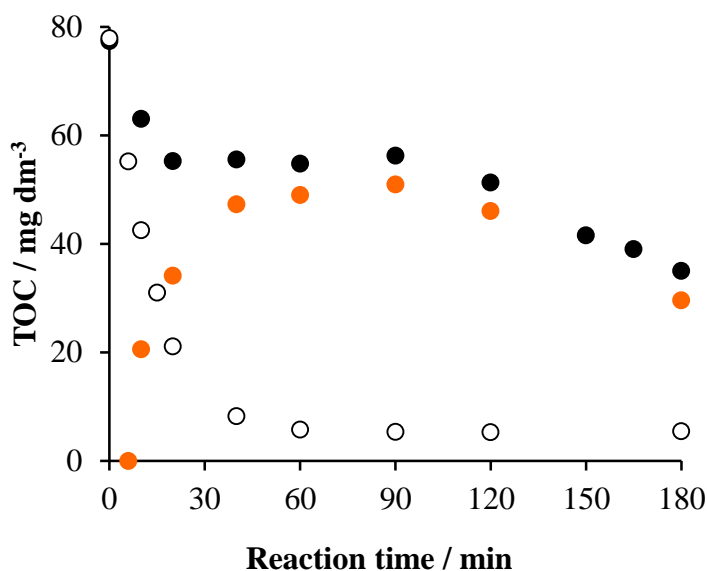
271 In this case, apparently, the increase of pH in the range studied enhanced the rate of mineralization.
 272 These results indicate that degradation of the intermediates formed in the primary processes is promoted
 273 by the hydroxide ions. Since a strong acidification was observed during the photocatalytic degradation
 274 of Triton X-100 (see section 2.2.), an increase of pH may enhance the driving force of the corresponding
 275 oxidation reactions of mineralization. On the basis of the plots in Figure 10, the most significant effect
 276 of pH can be observed in the first 25-30-min period of irradiation, where the rate of the TOC change is

the highest at each pH value. This phenomenon suggests that in this period mostly the species formed by the cleavage of the last member of the polyethoxylate chain are mineralized, obviously faster than those (bigger ones) formed in the fragmentation along the whole chain. Oxidation of these species takes place via formation of carboxylic acids, the deprotonation of which generates anions being not favored in the respect of adsorption on the negatively charged surface at $\text{pH} > 7$. Hence, the promoting effect of the increased pH may be attributed to the redox reactions of the intermediates containing 1 or 2 carbon atoms, in the solution phase.

2.5. Mechanistic considerations; intermediates

In order to get insight into the mechanism of the photocatalytic degradation and mineralization of Triton X-100, also some data regarding the intermediates formed were determined. Although the measured TOC values concern the whole reaction mixture, those belonging to the intermediates can also be determined. It is the difference of the TOC belonging to the overall system and that corresponding to the unreacted surfactant. The latter one can be calculated from the actual concentration of Triton X-100 measured by UHPLC. Figure 11 displays these TOC vs. time plots obtained for the air/UV/TiO₂ system.

Figure 11. The change of the TOC as functions of time in the system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and 1 g dm^{-3} TiO₂: for the whole system (●), for the unreacted surfactant (○), for the intermediates (●).

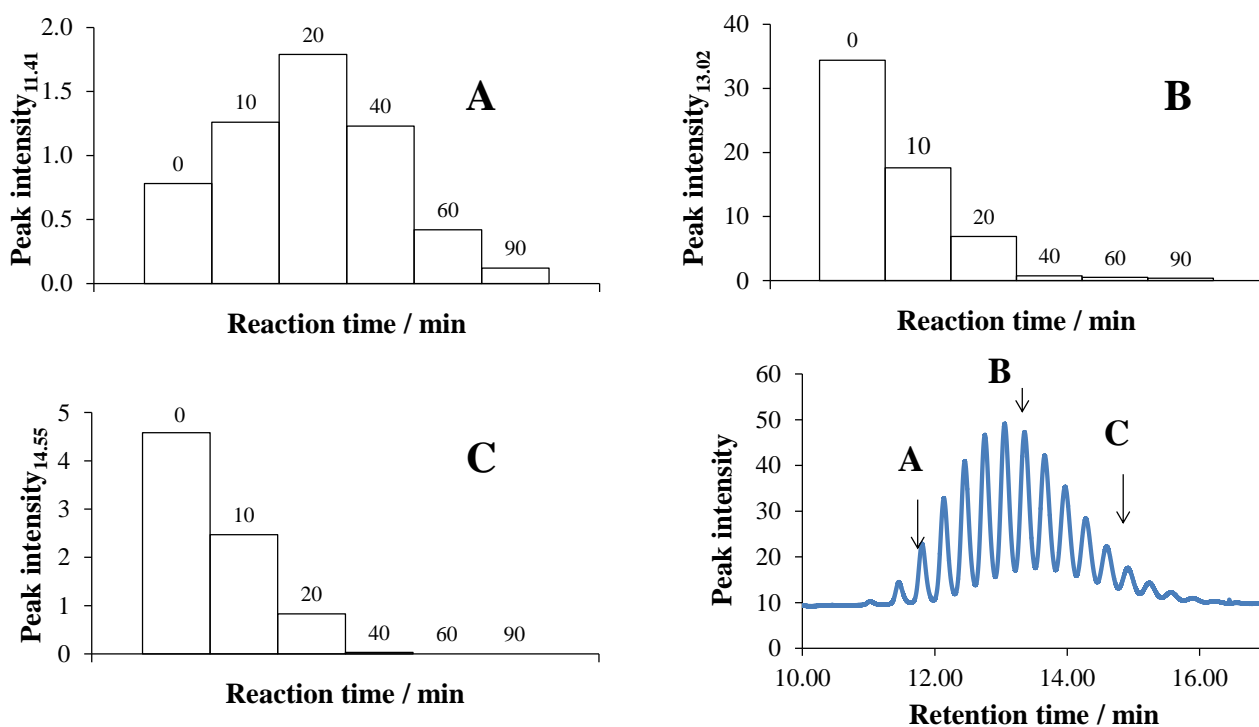


In the first 60 minutes the TOC representing the intermediates steeply increased, accompanied by the similarly fast and finally total disappearance of the starting surfactant. In the 60-120-minute period the TOC of the intermediates hardly changed, indicating that mostly their oxidation/oxygenation and cleavage took place. Subsequently their mineralization speeded up due to the oxidation of the short ethoxy chains.

2.5.1. UHPLC measurements

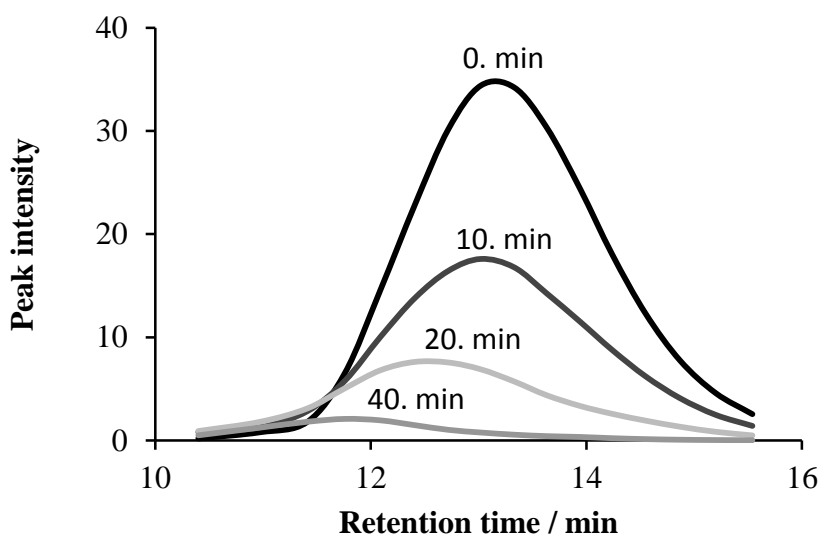
Since the UHPLC chromatogram of Triton X-100 consist of several peaks corresponding to the components with various lengths of ethoxy chains (Figure 12), its time-dependent change well demonstrates how the concentrations of these components are affected during the photocatalysis. The retention time of these non-ionic surfactant components is in strong correlation with the length of the ethoxy chain, i.e., the number of the ethoxy groups (n); longer chain corresponds to higher n . The column charts in Figure 12 (A, B, C) well demonstrate how the representative peaks (and, thus, the concentrations) of the components of different lengths change as functions of time. The peak intensity of the shorter-chain components (with retention times of 10.4-11.76 min) increased in the first 20 minutes of the reaction, then decreased (Figure 12 A). The peak intensity of the components with 12.09-14.24-minute retention time (Figure 12 B) decreased slower than that belonging to the long-chain components (with retention times of 14.55-15.87 min, Figure 12 C). The concentration of the latter group diminished below the detection limit already within 40 minutes.

Figure 12. The change of the peak intensity as functions of reaction time from the UHPLC chromatograms obtained during the photocatalysis of the system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and $1 \text{ g dm}^{-3} \text{ TiO}_2$: at the retention time of 11.41 min (A), 13.02 min (B), and 14.55 min (C).



Analyzing the chromatograms, the envelopes of the peak intensities belonging to different retention times after various reaction times were also plot (Figure 13). It is clearly seen that the retention time of the maximum peak intensity gradually decreased during the photocatalytic process, i.e., the components with longer chains degraded faster, also in accordance with the column charts in Figure 12.

329 **Figure 13.** The peak intensity as functions of retention time, taken from the UHPLC
330 chromatograms during the photocatalysis of the system containing 2×10^{-4} mol dm⁻³ Triton
331 X-100 and 1 g dm⁻³ TiO₂, after 0, 10, 20, and 40 min reaction time.
332



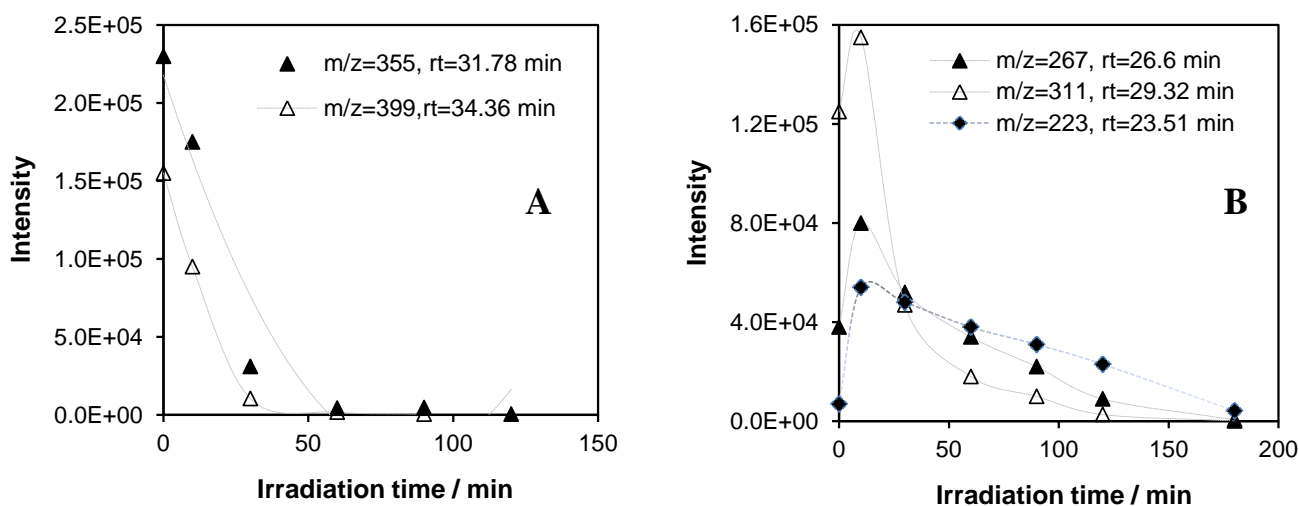
333 These results suggest that in the heterogeneous photocatalytic degradation of Triton X-100, under our
334 experimental conditions, the attack by hydroxyl radicals photogenerated is favored at the ethoxy side-
335 chain. This conclusion is confirmed by the change of the absorption spectrum (Figure 3); no shift of the
336 longer-wavelength (275-nm) band was observed, i.e., no hydroxylation of the aromatic ring took place.
337 After the total disappearance of the starting surfactant (after ca.60 min) an appreciable absorbance of the
338 275-nm band remained, which indicates that also intermediates with aromatic ring were formed during
339 the first hour. Further irradiation led to the cleavage of the aromatic ring, giving intermediates, which do
340 not absorb in the longer-wavelength range. In accordance with our observation, intermediates with
341 hydroxylated aromatic ring were not detected during the degradation of this non-ionic surfactant and
342 similar alkylphenol ethoxylates in other advanced oxidation procedures [34-38]. The lack of the
343 formation of intermediates with hydroxylated aromatic ring deviates from our earlier observations
344 regarding the photocatalytic degradation of benzenesulfonate and phenylalanine [28, **Hiba! A
345 könyvjelző nem létezik.**]. These results may be related to the facts that the efficiency for the
346 photocatalytic mineralization of the latter compounds was increased by ozonation in a synergistic way,
347 while in the case of Triton X-100 O₃ did not accelerate the TiO₂ mediated degradation.
348

349 2.5.2. GC-MS measurements

351 The UHPLC analysis did not give any information regarding the intermediates the structures of which
352 significantly deviate from those of the components of Triton X-100. Thus, in order to detect also such
353 intermediates, GC-MS measurements were also carried out after the solid-phase extraction as described
354 in the experimental section. Although this method is suitable only to the detection of species of lower
355 molecular weight, the tendencies observed for those can be generalized for the transformation of the
356 bigger components of Triton X-100.

357 The following figures present the intensity vs. irradiation time plots for the most abundant fragment
 358 ion of the species which could be identified unambiguously or with high probability on the basis of their
 359 mass spectra and retention times. (The ion chromatograms belonging to the different irradiation times
 360 and the mass spectra of typical components in the reaction mixture, identified by our GC-MS
 361 measurements, can be found in the supplementary material as Figures S3 and S4 , respectively.) Figure
 362 14A shows the starting components of Triton X-100 with ethoxylate number (n) of 5 and 6, i.e., with
 363 molecular weight of 426 and 470, respectively. The concentration of these components decreased from
 364 the very beginning of the irradiation, and practically disappeared within 40 minutes. However, the
 365 concentration of the components with $n = 2, 3$, and 4, i.e., with molecular weight of 294, 338, and 383,
 366 respectively, increased in the first 10 minutes, which was followed by a gradual decay. These results are
 367 in accordance with those of the UHPLC measurements, indicating that the fragmentation of the longer
 368 polyethoxylate chains of the starting components initially increased the concentration of those with
 369 shorter ones. **Notably, the m/z value corresponding to the most abundant fragment ion (i.e. the base peak)
 370 differs from the molecular weight (i.e. the m/z value of the mother peak) by 71 in each case in Figure
 371 14, indicating compounds of the same type of structure (i.e., $(\text{CH}_3)_3\text{C}-\text{CH}_2-(\text{CH}_2)_2\text{C}-\text{C}_6\text{H}_4-\text{O}-$
 372 $(\text{CH}_2\text{CH}_2\text{O})_n-\text{H}$), from which the fragment ion was formed by the loss of the pentyl (i.e. $(\text{CH}_3)_3\text{C}-\text{CH}_2-$
 373) group.**

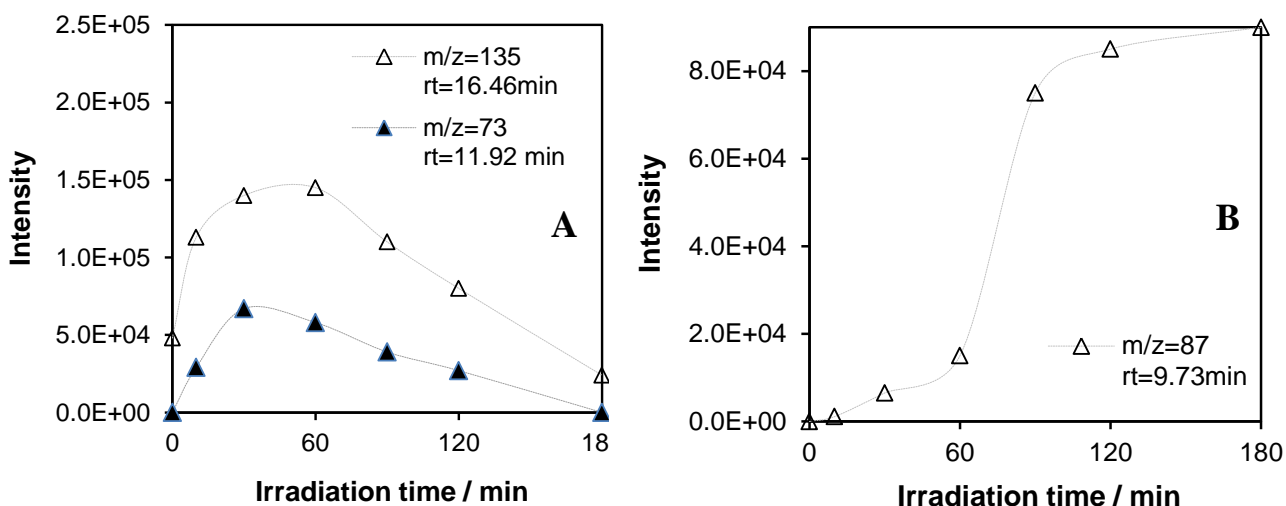
374
 375 **Figure 14.** Intensity vs. irradiation time plots for the most abundant fragment ion of the
 376 starting components of Triton X-100 with molecular weight of 470 ($m/z = 399$), 426 ($m/z =$
 377 355) (A), 382 ($m/z = 311$), 338 ($m/z = 267$), and 294 ($m/z = 223$) (B) in the photocatalysis
 378 of the system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and 1 g dm^{-3} TiO_2 .
 379



380
 381 The intensity vs. irradiation time plots for the most abundant fragment ion of characteristic
 382 intermediates detected by GC-MS are shown in Figure 15. As it can be seen, not only the molecular
 383 weights, but also the corresponding retention times are significantly smaller than those of the starting
 384 components (even if of lower n values). The maximum concentration of them belong to longer times,
 385 moreover, the smallest one (Figure 15B) is the most abundant intermediate detected by this method after

180-min irradiation. As to the structure of these intermediates, $M=206$ ($m/z=135$, Figure 15A) could be unambiguously identified as 4-(1,1,3,3-tetramethylbutyl)phenol, i.e., the alkylphenol (= octylphenol) part of the starting components of Triton X-100. This is the result of the total cleavage of the polyethoxylate chains without any oxidation of the common rest of the original tensid molecules. In this case too, similarly to the mass spectra of the starting components, the m/z value of the base peak differs from that of the mother peak by 71, due to the loss of the same pentyl group.

Figure 15. Intensity vs. irradiation time plots for the most abundant fragment ion of characteristic intermediates with molecular weight of 206 ($m/z = 135$), 148 ($m/z = 73$) (A), and 118 ($m/z = 87$) (B) in the photocatalysis of the system containing $2 \times 10^{-4} \text{ mol dm}^{-3}$ Triton X-100 and $1 \text{ g dm}^{-3} \text{ TiO}_2$.



The time dependence of the concentration of this intermediate indicates that it can be formed in a relatively early stage of the photocatalysis, obviously from the starting components with shorter ethoxylate chains, and later also from those with longer chains. Thus, the decay of this intermediate lasts till the end of the 3-hour irradiation period.

The other plot in Figure 15A can be assigned to $\text{HO}(\text{CH}_2\text{CH}_2\text{O})_2\text{CH}_2\text{CHO}$ ($M=148$, the base peak of $m/z=73$ belongs to the $-\text{CH}_2\text{OCH}_2\text{CHO}$ fragment), which is clearly derived from the ethoxy chain of the starting molecules via fragmentation. Thus, it is a kind of complementary intermediate of the octylphenol part previously discussed. Both are the results of the same type of fragmentation. Formation of these intermediates is in full accordance with the results recently obtained by LC-ESI-MS method [23].

Oxidation of these species led to other intermediates of various structures, the identification of which needs further investigations. As our UV (absorption and emission) spectral study indicated (see section 2.1.), they involve ring-opened compounds too, in agreement with the results of GC-MS analysis regarding the photocatalysis of different alkylphenols [24]. Nevertheless, the intermediate, for the most abundant fragment ion of which the intensity vs. time plot is given in Figure 15B, may be assigned as a short-chain (with carbon number of 5) hydroxy carboxylic acid or ester. Its complete oxidation (i.e. total mineralization) would need an extended irradiation.

3. Experimental Section

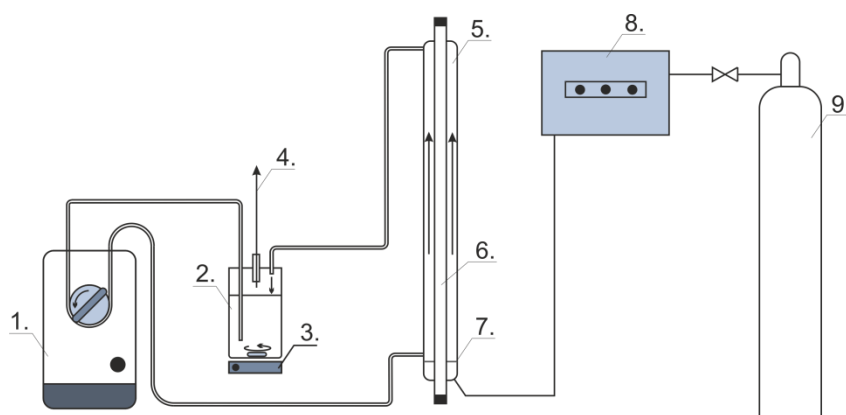
3.1. Materials

In all experiments of this work, the titanium dioxide catalyst used was Degussa P25 (70% anatase, 30% rutile; with a surface area of $50 \text{ m}^2 \text{ g}^{-1}$). The concentration of TiO_2 was 1 g dm^{-3} . All other materials such as $\text{Na}_2\text{S}_2\text{O}_8$ (Merck) and Triton X-100 (Alfa Aesar) were of reagent grade. Its concentration was $2 \times 10^{-4} \text{ mol dm}^{-3}$ ($= 0.126 \text{ g dm}^{-3}$) in each degradation experiments. Compressed air was bubbled through the reaction mixtures from gas bottles, serving for both stirring and (with its O_2 content) as electron acceptor. O_3 was produced by a LAB2B ozone generator, and introduced in the same air stream. In all of these experiments, ozone dosage was adjusted to $3.5 \times 10^{-4} \text{ min}^{-1}$. High purity water used as solvent in this study was double distilled and then purified with a Milli-Q system. In order not to disturb the subsequent analyses, no buffer was used in the reaction mixtures to be irradiated.

3.2. Photochemical experiments

Photochemical experiments were carried out in a laboratory-scale reactor with an effective volume of 2.5 dm^3 . The heterogeneous reaction mixture (TiO_2 suspension) was circulated by using a peristaltic pump through the reactor and the buffer vessel and by continuously bubbling air with a flow rate of $40 \text{ dm}^3 \text{ h}^{-1}$ within the reactor. The photon flux of the internal light source (40W, $\lambda_{\text{max}} = 350 \text{ nm}$, i.e., UVA range) was measured by tris(oxalato)ferrate(III) chemical actinometry [39,40] It was estimated to be $4.3 \times 10^{-6} \text{ mol photon dm}^{-3} \text{ s}^{-1}$.

Figure 16. Sketch of the photocatalytic reactor with the auxiliary units: 1. peristaltic pump 2. buffer vessel 3. magnetic stirrer 4. sampling port 5. reactor (pyrex vessel) 6. light source 7. porous sieve 8. ozone generator 8. gas cylinder.



436

3.3. Analytical procedures

For analysis, 4 cm^3 samples were taken with a syringe from the reactor through a septum. The solid phase of samples, when necessary, was removed by filtration using Millipore Millex-LCR PTFE $0.45 \mu\text{m}$ filters. The pH of the aqueous phase of the reaction mixture was measured with SEN Tix 41 electrode.

441

442 Degradation of Triton X-100 was followed by 1290 Infinity UHPLC system (Agilent Technologies),
443 equipped with binary gradient pump, automatic injector, column thermostat, DAD detector, and
444 Chemstation data acquisition system. Band profiles of Triton X-100 were recorded at 223 nm. The
445 column used during the experiments was a 100x2 mm Synergy HydroRP C18 (Phenomenex, Torrance,
446 CA, USA) column packed with 2.5 μm particles. Column was thermostated at 50°C. The eluent flow
447 rate was 1 $\text{cm}^3 \text{min}^{-1}$. Composition of mobile phase was 65:35 methanol:water for five minutes of
448 analysis, and it was changed to 75:25 in the next five minutes.

449 The individually identifiable organic compounds of the liquid samples were determined by gas
450 chromatography–mass spectrometry method. During the sample preparation 4 cm^3 solution sample was
451 extracted with 6 cm^3 of chloroform (Chromasolv). During the extraction the two phases were shaken for
452 20 minutes. After the two phases separated, the extract was filtered with a 0.45 μm syringe filter and
453 gently evaporated to dryness in nitrogen gas flow, then re-dissolved in 60 μl chloroform. The as prepared
454 samples were analysed by gas chromatography–mass spectrometry (GC-MS). The injector was 270 °C.
455 The separation was carried out on an Agilent 6890N gas chromatograph with Agilent DB-5ms UI column
456 (30 m \times 0,25 mm \times 250 μm). As a detector we used an Agilent 5973 N type mass spectrometer in scan
457 mode ($m/z=33\text{-}550$). The ion source switched on with a 5 minute delay from startup (= solvent delay).
458 The temperature program for the separation was as follows: the initial column area was set to 60 °C and
459 kept there for 1 minute. Then the temperature was raised to 310 °C at 8 °C/min and held for an additional
460 5 minutes. The temperature of the Aux (= column-MS interface) was 280 °C. As a mobile phase high
461 purity helium was used with 1 ml/min flow rate. ~1 μl sample was injected to the column without
462 dividing the sample flow (splitless).

463 Ozone concentration was determined by iodometry, using sodium iodide as reagent and sodium
464 thiosulfate for the titration of the iodine formed [41].

465 The absorption and emission spectra were recorded with a Specord S 100 diode array
466 spectrophotometer and a Perkin_Elmer LS 50B spectrofluorometer, respectively, using quartz cuvettes
467 of various pathlengths. Mineralization was followed by measuring the total organic carbon (TOC)
468 concentration, by application of a Thermo Electron Corporation TOC TN 1200 apparatus.

469 4. Conclusions

470 Triton X-100 as the most widely applied representative of alkylphenolethoxylate type non-ionic
471 surfactants was degraded and mineralized by TiO_2 mediated heterogeneous photocatalysis. As other
472 advanced oxidation procedures, ozonation and treatment with peroxydisulfate were also investigated
473 under the same conditions for comparisons. Besides, the combination of these advanced oxidation
474 procedures (AOPs) with photocatalysis were also studied. While TiO_2 mediated heterogeneous
475 photocatalysis proved to be an efficient method for the mineralization of this surfactant, its combination
476 with the other AOPs did not increase the degradation and mineralization rate. These results deviate from
477 those observed earlier for the treatment of ionic surfactants, and may be attributed to a different
478 mechanism in which no hydroxylation of the aromatic rings takes place. Monitoring the progress of
479 photocatalytic mineralization of the Triton X-100 components by GC-MS, both starting tensid molecules
480 and intermediates formed via fragmentation were followed. While cleavage of the polyethoxylate chain

481 took place in the early stage of the photocatalytic process, the alkyl part of the tensid molecules was
482 mineralized much slower.

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488 Author Contributions

489 The present paper is based on the research work of Péter Hegedűs supervised by Erzsébet Szabó-
490 Bárdos and Krisztián Horváth. Péter Hajós was involved in the UHPLC measurements. Ottó Horváth
491 contributed to the interpretation of the results and prepared the manuscript.

492 Conflicts of Interest

493 The authors declare no conflict of interest.

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497

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